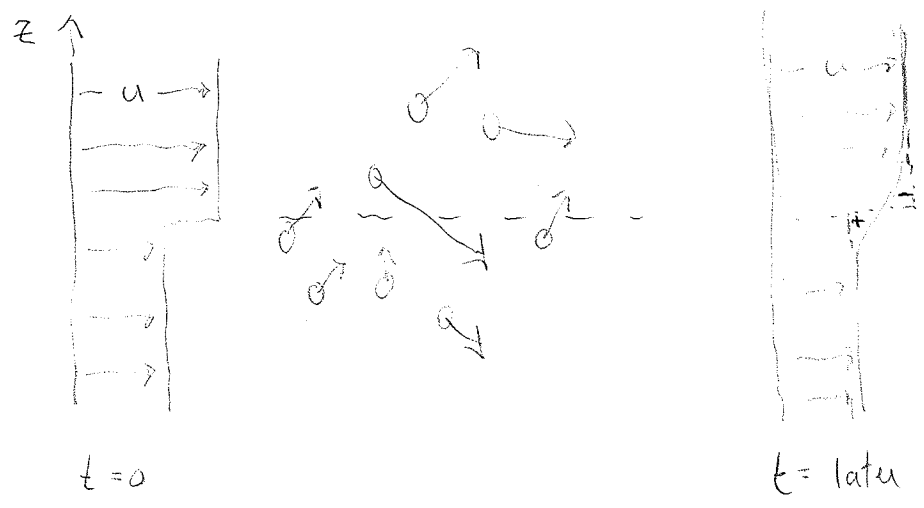


III.2 VISCOSITY Continued...

(1)

You can also think of this as arising from molecular diffusion of momentum:



NOTE =
 "flux" = rate of advection/diffusion/transmission of a property across a surface, per unit area

z-direction flux of x-momentum = $-\mu \frac{\partial u}{\partial z}$
 $\left[\frac{\text{kg m}}{\text{s}} \frac{1}{\text{s}} \frac{1}{\text{m}^2} \right] = \left[\frac{\text{kg}}{\text{m s}^2} \right] = \left[\frac{\text{N}}{\text{m}^2} \right]$

more generally define

$\underline{F}^x =$ \vec{x} direction flux of x-momentum = $-\mu \nabla u$

rate per unit area property is momentum

then the viscous force on a parcel is

$$\text{Visc. Force}^x = \int_A -\underline{F}^x \cdot \hat{n} dA \quad \stackrel{\text{using Gauss Divergence Thm.}}{=} \quad \int_V -\nabla \cdot \underline{F}^x dV$$

\hat{n}
 A
 net inward flux of momentum (or net viscous stress on A)

and in the limit $V \rightarrow 0$

$$\frac{\text{Visc. Force}^x}{\text{unit volume}} = -\nabla \cdot \underline{F}^x = \mu \nabla \cdot \nabla u = \mu \nabla^2 u \quad \text{again}$$

Summarizing: the equations of motion may be written as

x mom $\frac{Du}{Dt} = -\frac{1}{\rho} p_x + \nu \nabla^2 u$

y mom $\frac{Dv}{Dt} = -\frac{1}{\rho} p_y + \nu \nabla^2 v$

z mom $\frac{Dw}{Dt} = -\frac{1}{\rho} p_z - g + \nu \nabla^2 w$

mass $\frac{1}{\rho} \frac{D\rho}{Dt} + \nabla \cdot \underline{u} = 0$

conservation of momentum unit mass

where $\nu \equiv \frac{\mu}{\rho} = \text{"kinematic viscosity"} \quad [m^2 s^{-1}]$

at 20°C, $p = 1 \text{ atm.}$

	$\nu [m^2 s^{-1}]$	$\rho [kg m^{-3}]$
air	1.5×10^{-5}	~ 1.2
water	1.0×10^{-6}	~ 1000

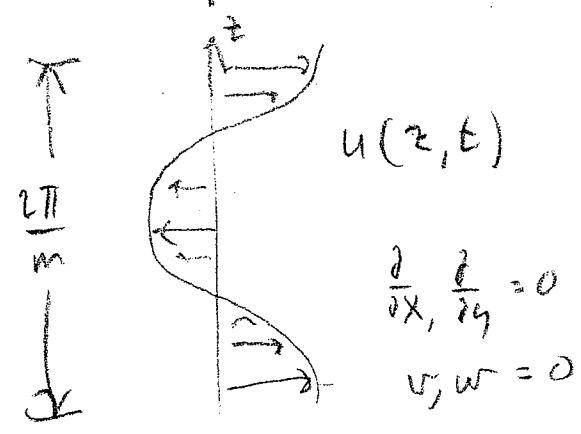
Note: a complete derivation includes a viscous term proportional to $\nabla \cdot \underline{u}$ but few flows have viscosity & compressibility important at the same time

Exact: KC 4.6 stress tensor
KC 4.7 mom. conservation

KC 4.10 viscosity w/ $\nabla \cdot \underline{u} \neq 0$ for a true Newtonian fluid

Example: viscosity gets rid of variations in velocity (3)

consider a flow line



x mm

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right)$$

so $u_t = \nu u_{zz}$ (like a "heat equation")

if $u(t=0) = u_0 \cos(mz)$

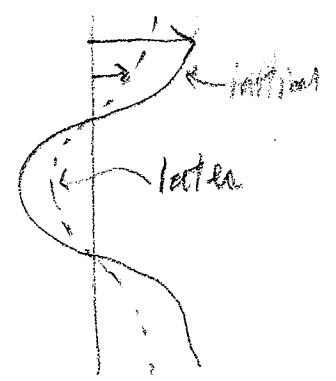
guess $u = \mathcal{U}(t) \cos(mz)$ [trying separation of variables]

$$\Rightarrow \frac{\partial \mathcal{U}}{\partial t} + \nu m^2 \mathcal{U} = 0$$

$$\Rightarrow \mathcal{U} = u_0 e^{-\nu m^2 t}$$

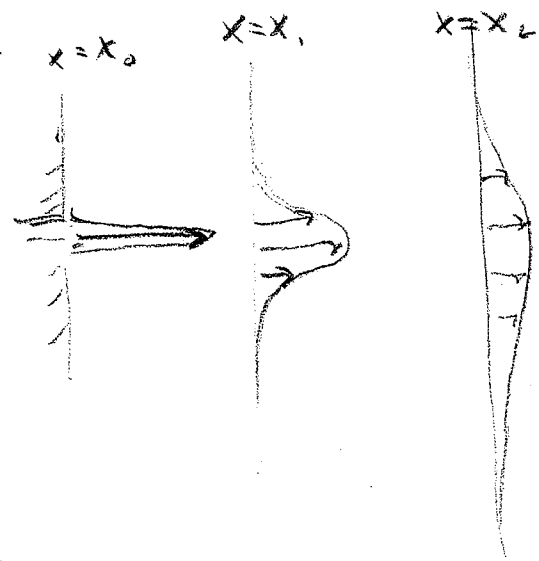
full solution $u = u_0 e^{-\nu m^2 t} \cos(mz)$

- viscosity weakens the layered flow



Example 2

Jet

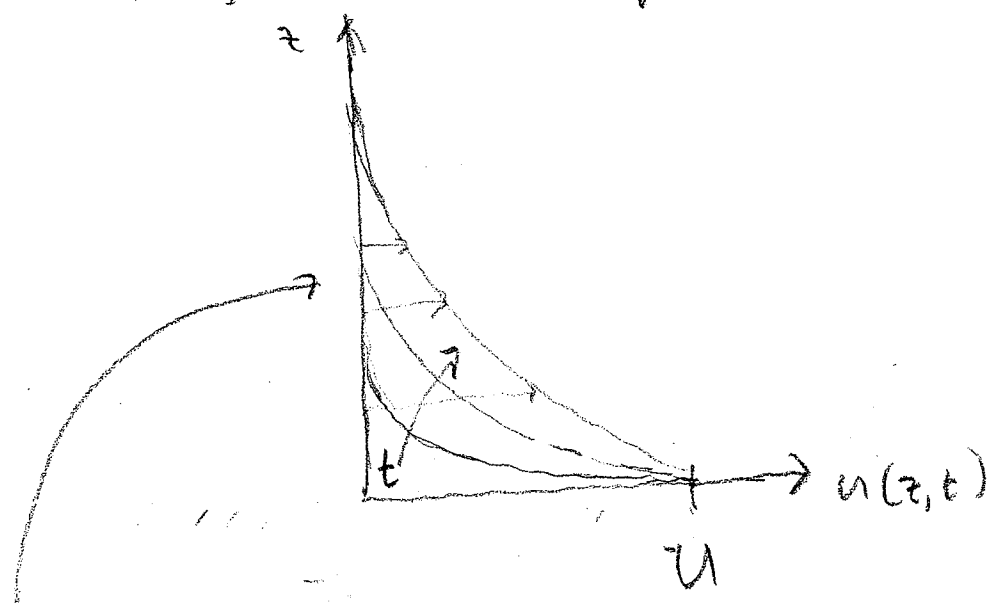


Viscosity makes
jet grow broader
and weaker

Example 3

Boundary Layer: Start moving a boundary near

$u=0$ initially



TTTTT
 $u=U$

region of viscous
acceleration of fluid
grows thicker over time

scaling $u_t = \nu u_{zz} \Rightarrow L \propto \sqrt{\nu t}$

$\frac{u}{U}$

For water at 20°C $D = 10^{-6} \text{ m}^2 \text{ s}^{-1}$



5

to in 10^2 sec

$$L = \sqrt{10^{-6} \frac{\text{m}^2}{\text{s}} \cdot 10^2 \text{ s}} = \sqrt{10^{-4} \text{ m}^2} = 1 \text{ cm}$$

(note: doesn't depend on the actual velocity!)