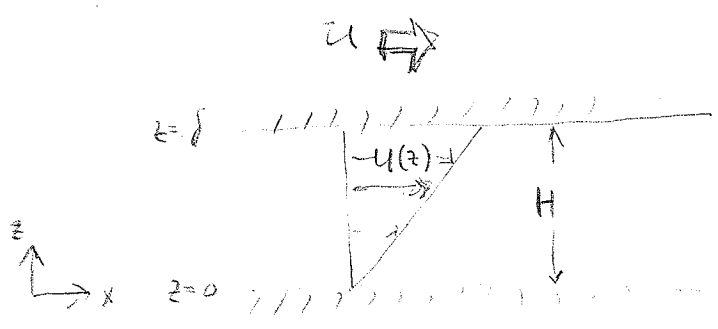


VISCOSITY

III.1

10/23/2009 (1)



Two plates w/ fluid between
 Top plate moving at speed u
 ("Couette Flow")

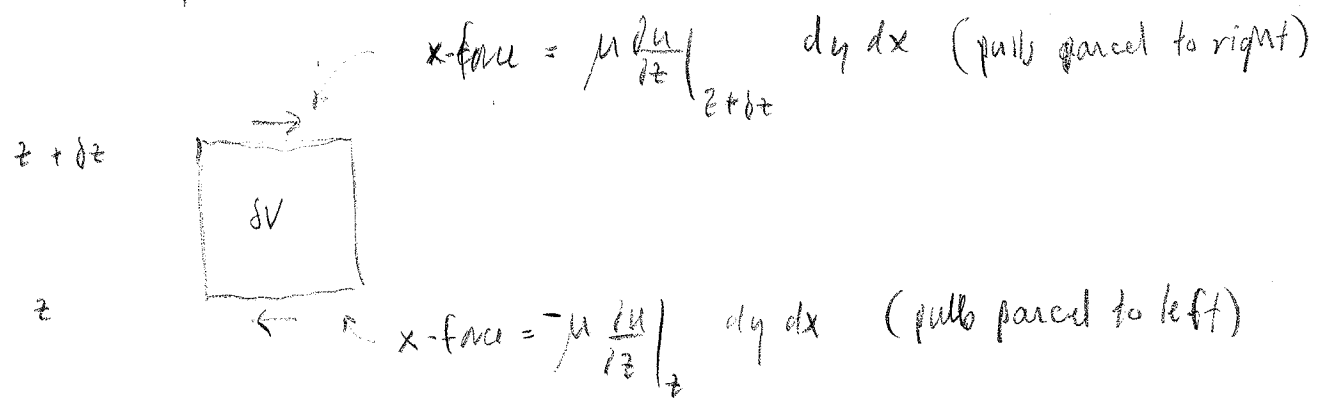
For real fluids we observe:

$u(0) = 0$ "No slip condition"
 $u(H) = u$

Force required to keep upper plate in motion
 unit horizontal area = $\mu \frac{u}{H} = \mu \frac{du}{dz} = \text{"shear stress"}$

μ = dynamic viscosity " $\left[\frac{\text{kg}}{\text{m s}} \right]$ This defines a "Newtonian Fluid"

Considering just a fluid parcel (with just $\partial u / \partial z$)



$\Rightarrow \frac{\text{Viscous Force}}{\text{unit vol}} = \lim_{\delta V \rightarrow 0} \left\{ \frac{1}{dx dy dz} \left(\mu \frac{\partial u}{\partial z} \Big|_{z+\delta z} - \mu \frac{\partial u}{\partial z} \Big|_z \right) dx dy \right\} = \frac{\partial}{\partial z} \mu \frac{\partial u}{\partial z}$

due to $\mu \frac{\partial^2 u}{\partial z^2}$ only

- in general we may neglect spatial variation of μ
- the relation stress = $\mu \cdot$ shear with $\mu = \text{const.}$ defines a "Newtonian fluid"
- Non-Newtonian fluids: μ may be a function of shear
 - shear thinning fluids: ball point pen ink, ketchup
 - "thickening": Silly Putty
- can have eq. $\mu = \mu(\text{temperature})$ + still be "Newtonian"

Generalizing the viscous force on a fluid parcel

$$\frac{\text{Visc. Force}^x}{\text{unit vol}} = \mu (u_{xx} + u_{yy} + u_{zz}) = \mu \nabla^2 u = \mu \nabla \cdot (\nabla u)$$

(similar expressions y + z)