

Femlab Models Used to Test Correlations of Evaporation Rates From Surfaces



Scope of Research

- ❑ Pesticides sprayed on a field
- ❑ Chemicals in an open channel
- ❑ Spilled chemicals





Background

- Evaporation of substances depends on:
 - Physical properties of substances – D , v , ρ
 - Concentration C_o
 - Surface Area
 - Atmospheric conditions
 - Wind speed
 - Approach concentration C_∞

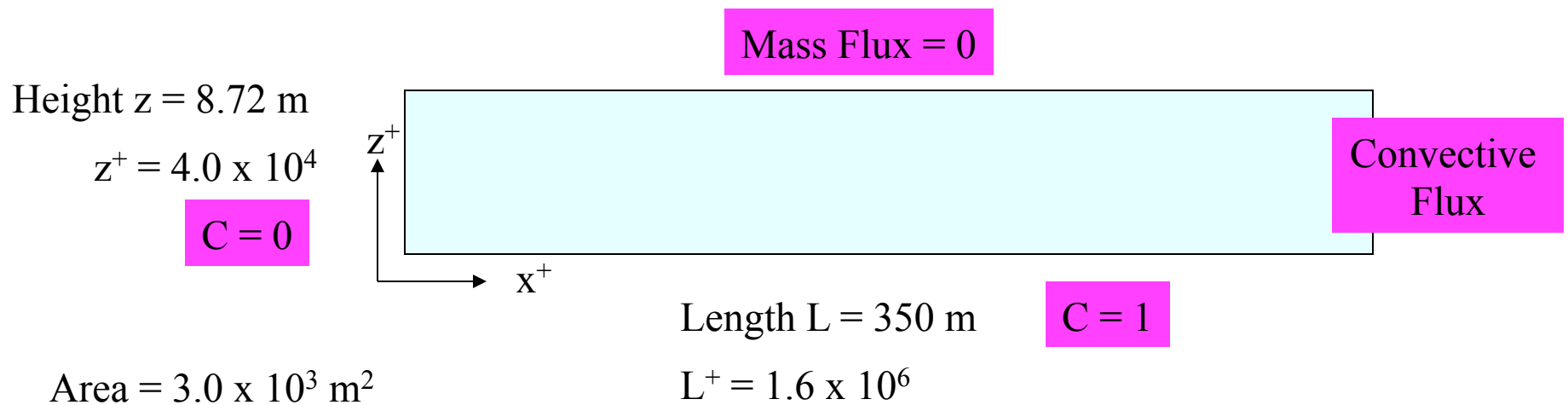
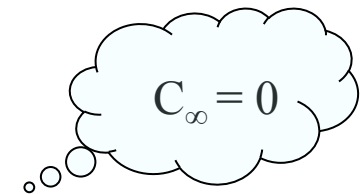


Femlab Solution

- Solved Using Femlab
- Results compared to:
 - Sleicher's article , I&EC Fund. **25** 659 (1986).
 - *Vaporization and Dispersion from a Surface to a Turbulent Boundary Layer*
 - Barry's article, , CEP, , p. 32, Jan. (2005)
 - *Estimation Rates of Spreading and Evaporation of Volatile Liquids*

Setup

- Large field
- Non dimensional variables



Theory Equations

□ Continuity Equation- $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial z} = 0$

□ Equation of Motion for turbulent flow- $u \frac{\partial \bar{c}}{\partial x} + v \frac{\partial \bar{c}}{\partial z} + \frac{\partial \overline{wc}}{\partial z} = D \frac{\partial^2 \bar{c}}{\partial z^2}$

□ Dimensionless Variables-

$$u^+ = \frac{u}{u_*} \quad x^+ = \frac{u_* x}{\nu} \quad z^+ = \frac{u_* z}{\nu}$$

Schmidt and Sherwood numbers

- Schmidt number, Sc is ratio of kinematic viscosity to diffusivity

$$Sc = \frac{\nu}{D}$$

- Sherwood number Sh_L is dimensionless concentration gradient at a surface

$$Sh_L = \frac{\bar{k}L}{D}$$

- Sherwood number is related to mass flux

$$N = \bar{k}A(C_0 - C_\infty)$$

Equations used in Femlab

□ Governing equation

- Convection and diffusion
- Steady-state

$$u^+ \frac{\partial \theta}{\partial x^+} = \frac{1}{Sc} \frac{\partial}{\partial z^+} \left(1 + Sc \frac{\epsilon_m}{\nu} \right) \frac{\partial \theta}{\partial z^+}$$

□ Eddy-diffusivity

$$\begin{aligned} 0 < z^+ < 45 : & \quad \frac{\epsilon_m}{\nu} = \frac{0.00090 z^{+3}}{[1 + 0.0067 z^{+2}]^{1/2}} \\ z^+ \geq 45 : & \quad \frac{\epsilon_m}{\nu} = 0.4 z^+ \end{aligned}$$

□ u^+ is x-velocity

$$\begin{aligned} z^+ < 10 : & \quad u^+ = z^+ \\ z^+ \geq 10 : & \quad u^+ = 5.1 + 2.5 \ln(z^+) \end{aligned}$$

Equations used in Sleicher' s and Barry' s

- Sleicher- dependent on Schmidt number and field size

$$Sh_x = 0.81(Sc * x^+)^{1/3} [1 + G(x^+)]^\alpha$$

$$G = 0.022 + 0.00081 \ln(Sc)$$

$$\alpha = 0.38 + 0.014 \ln(Sc)$$

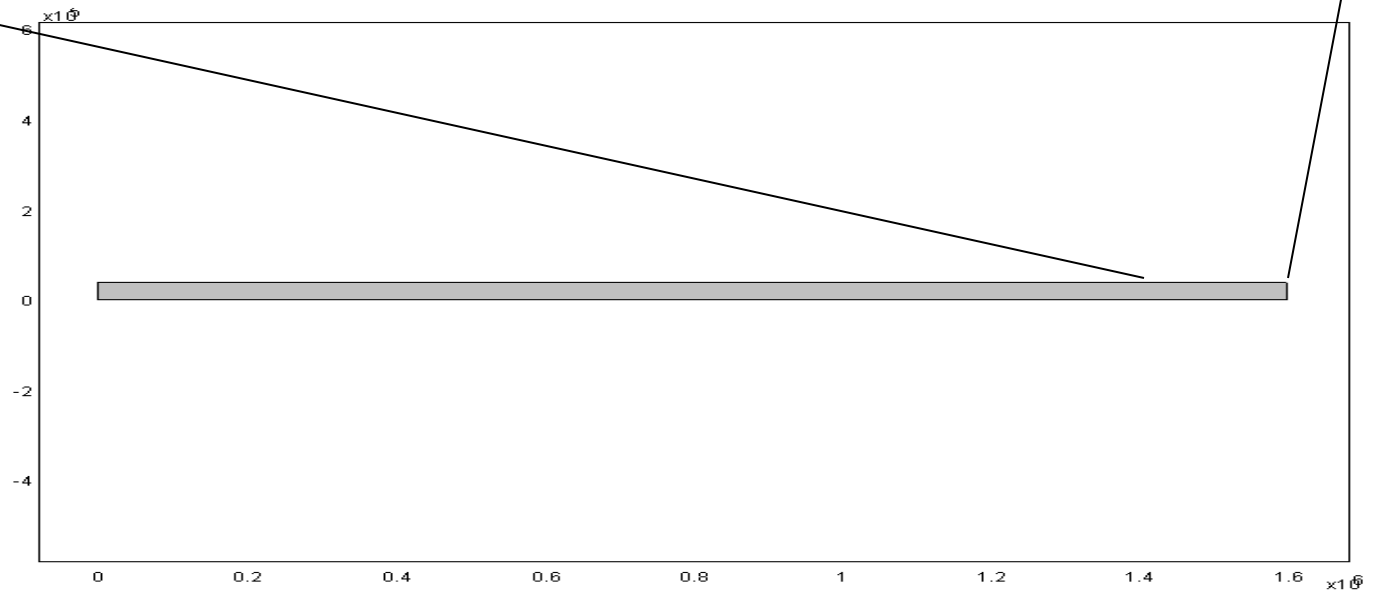
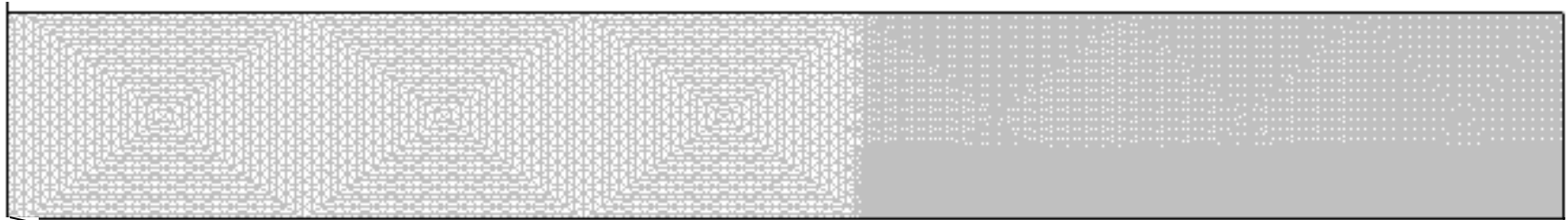
- Barry - dependent on Reynolds number and Schmidt number

$$Sh_x = 0.0365(Re_x)^{4/5} (Sc)^{1/2}$$

$$Re_x = \frac{u\rho x}{\mu}$$

Mesh Defined

Number of boundary elements	1648
Number of elements	125366
Minimum element quality	0.70
Number of degrees of freedom	252381



Assumptions

- Properties equivalent to air

Properties of Substance	
ρ (kg/m ³)	1.186
u (m/s)	2
ν (m ² /s)	1.57E-05
D (m ² /s)	5.20E-06
μ (kg/ m s)	1.84E-05

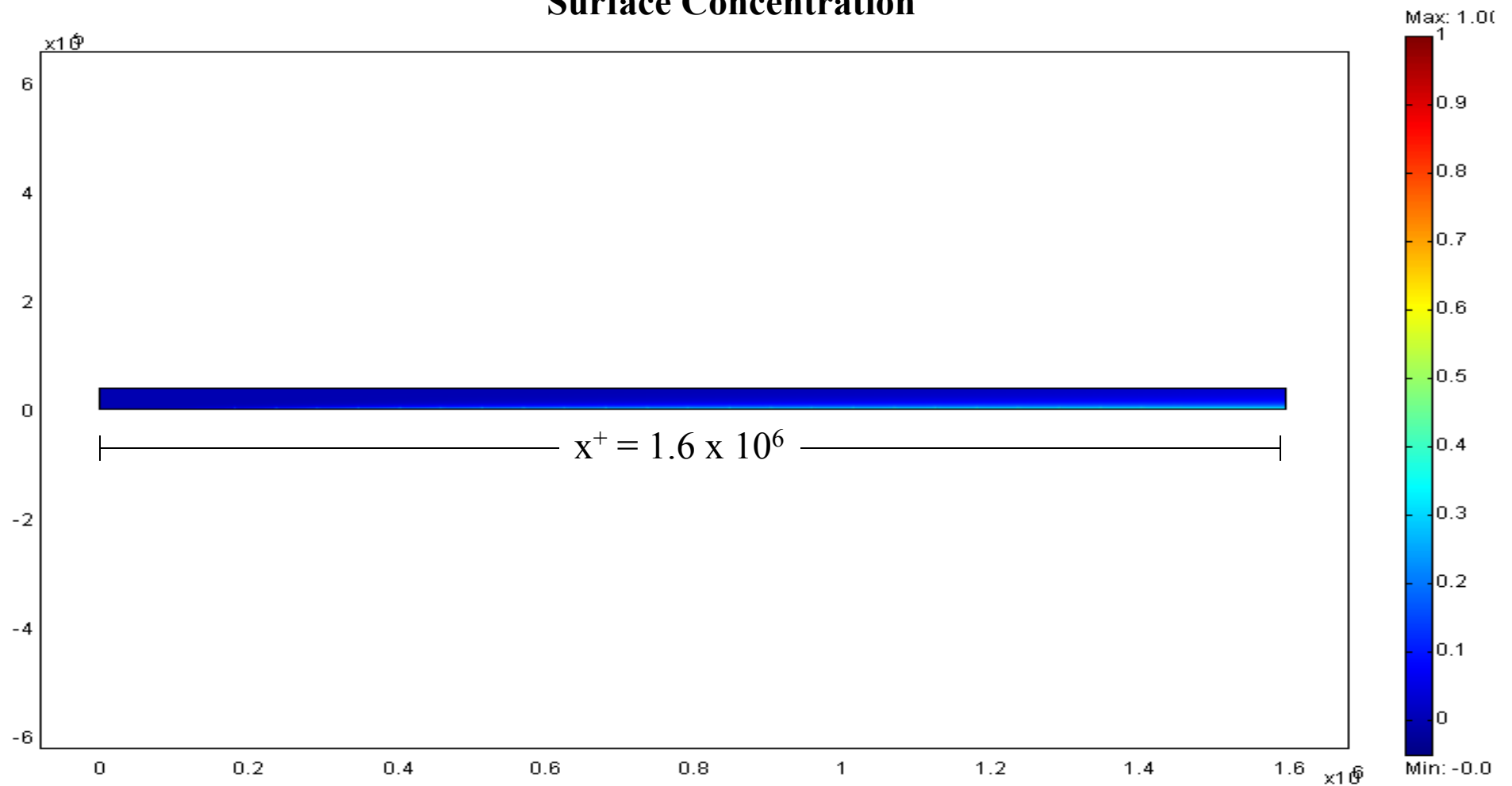
Field Properties	
L^+	1.60E+06
z^+	4.00E+04
L (m)	3.49E+02
z (m)	8.72E+00

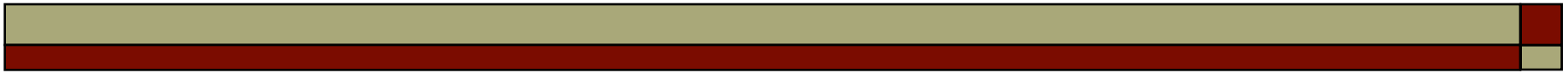
- Turbulent Flow $Re = 4.51 \times 10^7$

- Femlab & Sleicher- Turbulent boundary layer assumption – negligible
- Barry - Turbulent boundary layer regime

Concentration Profile – Entire Length

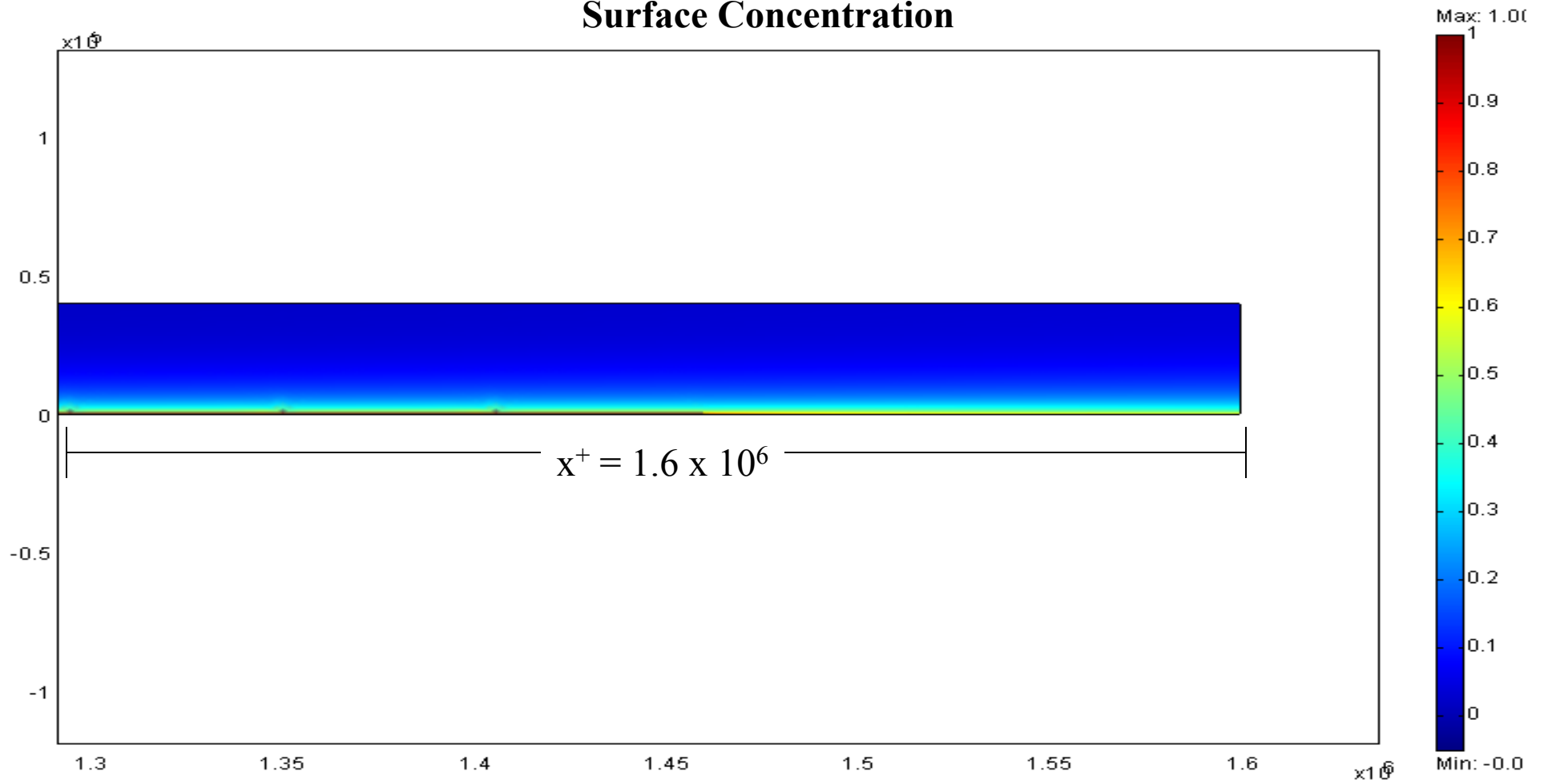
Surface Concentration





Concentration Profile

Surface Concentration



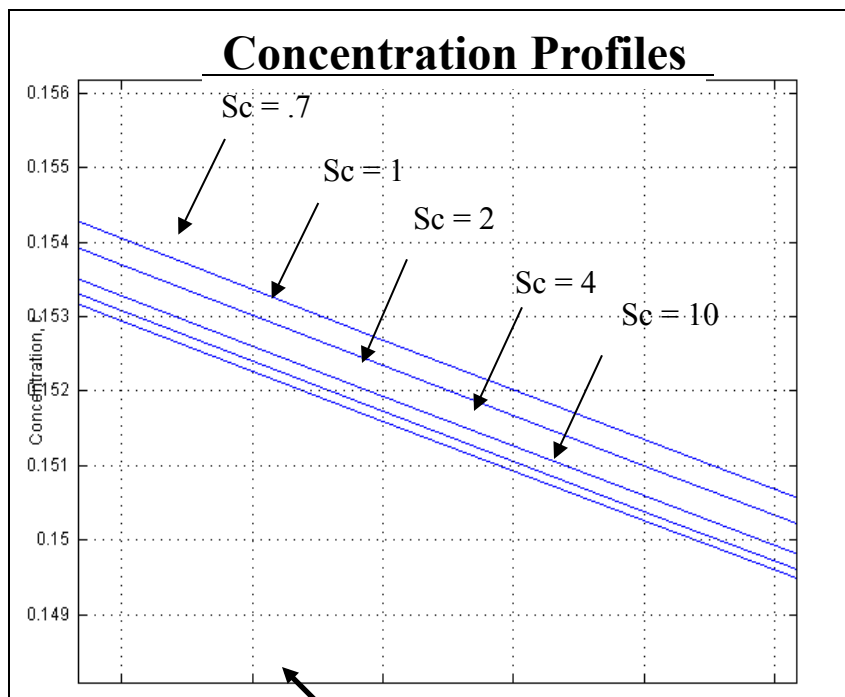
Results – Sherwood numbers

Sherwood numbers at $x^+ = 1.6 \times 10^6$

Sc	Femlab	Barry	Sleicher
0.7	4995	4.05×10^4	426
1	5045	4.85×10^4	570
2	5104	6.85×10^4	980
4	5134	9.69×10^4	1646
10	5153	1.53×10^5	3182

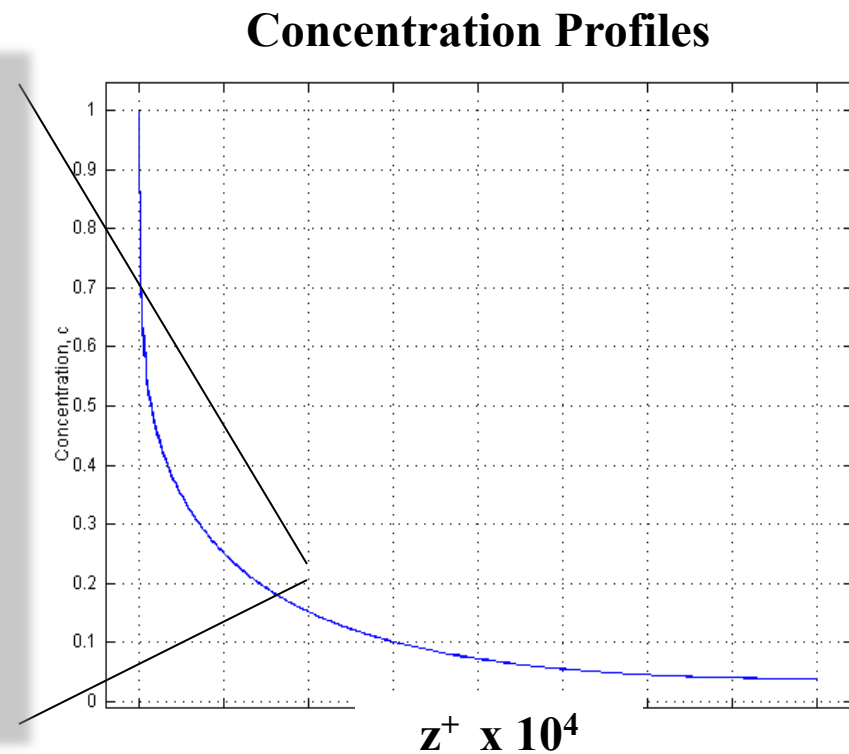
$$Sh_L = \frac{\bar{k}L}{D} \quad N = \bar{k}A(C_0 - C_\infty)$$

Varying Schmidt numbers at $x^+ = 1.6 \times 10^6$



June 3, 2005

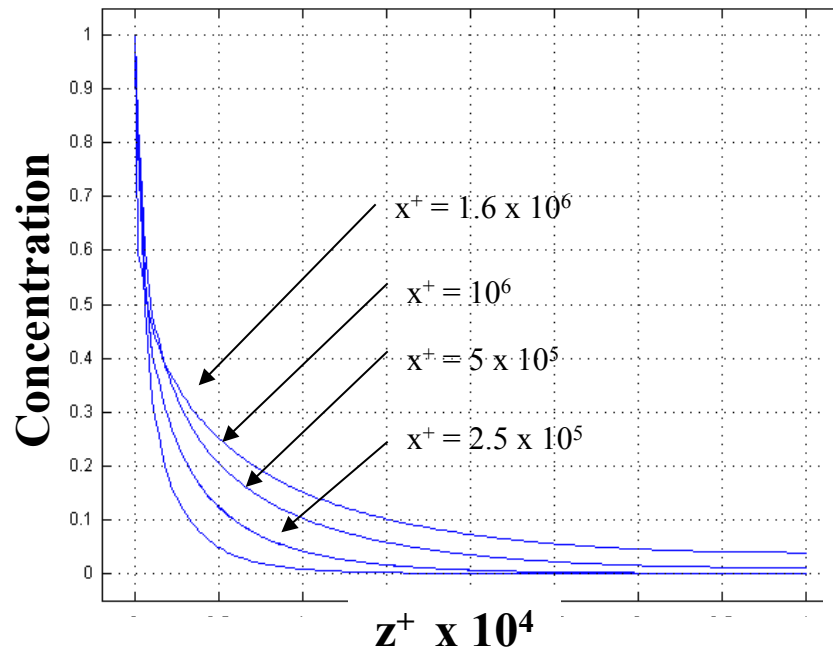
$z^+ \times 10^4$
Range: 0.99 – 1.015



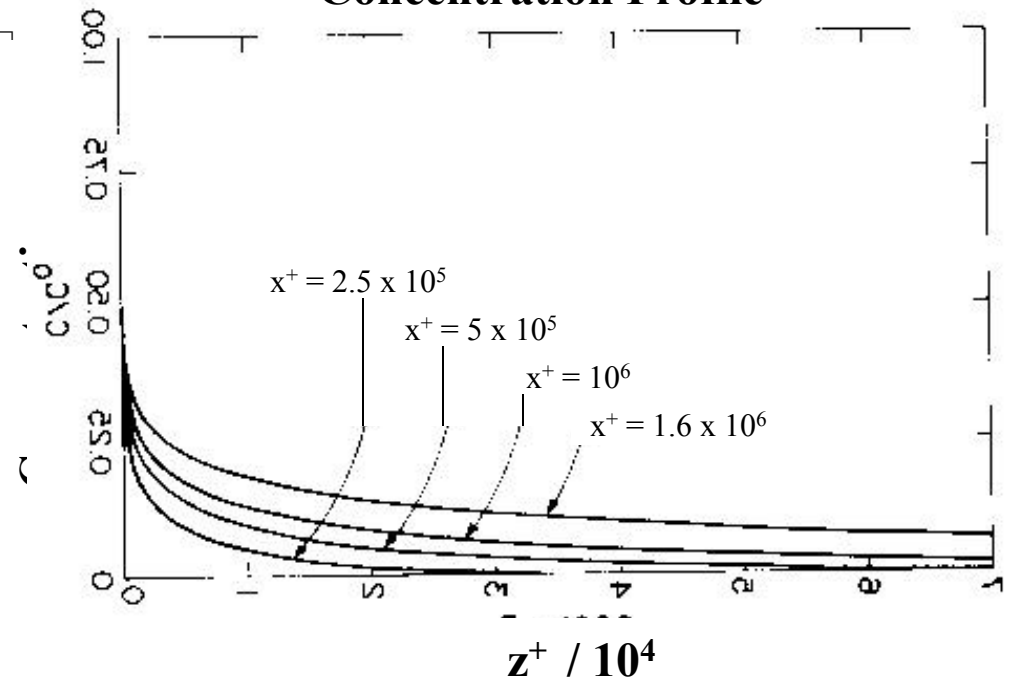
Range: 0 – 4×10^4
Final Concentrations $\sim 5 \times 10^{-3}$

Concentration Profiles for varying x^+

Femlab Results
Concentration Profile



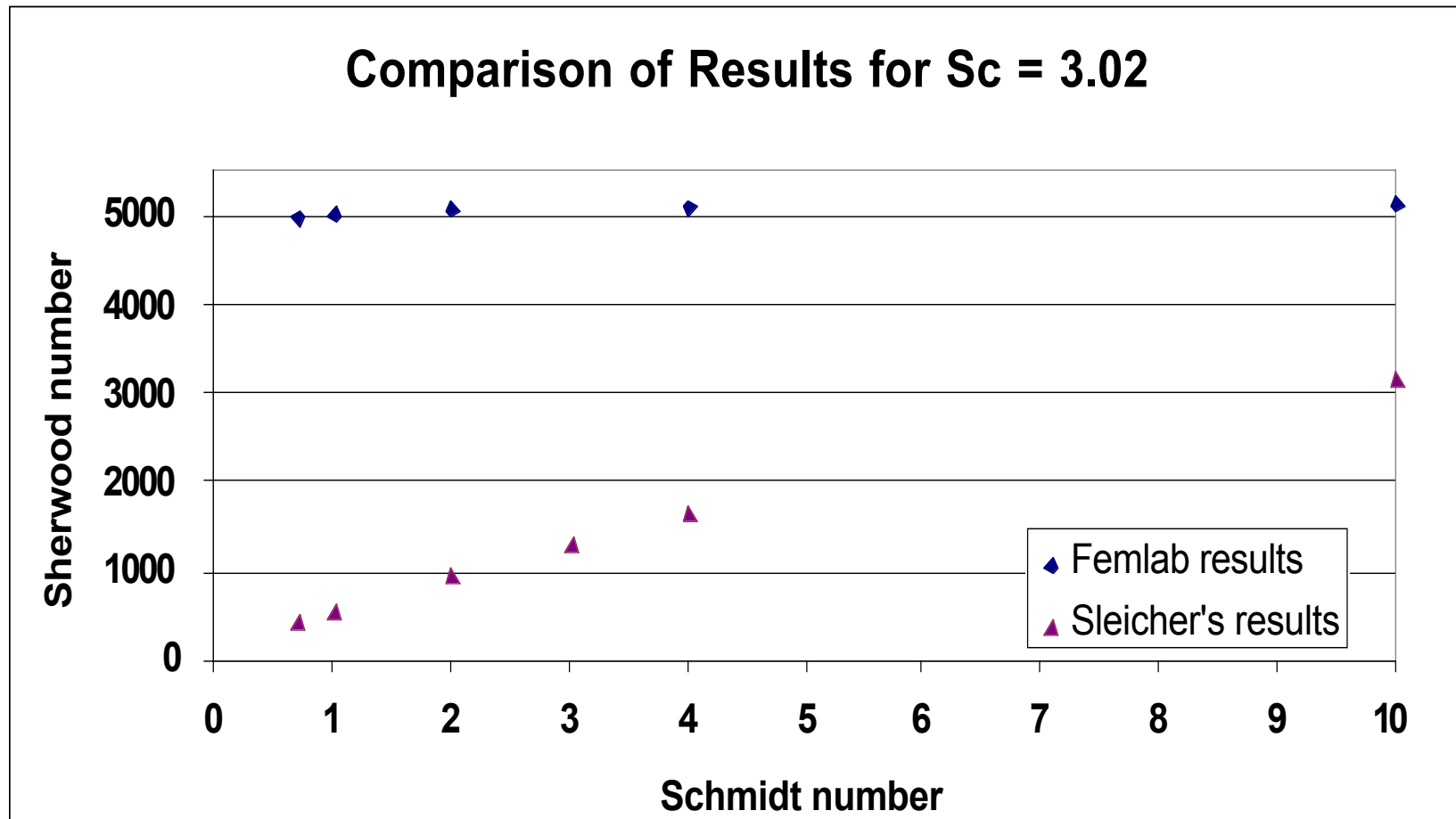
Sleicher's Data
Concentration Profile



Same Correlation

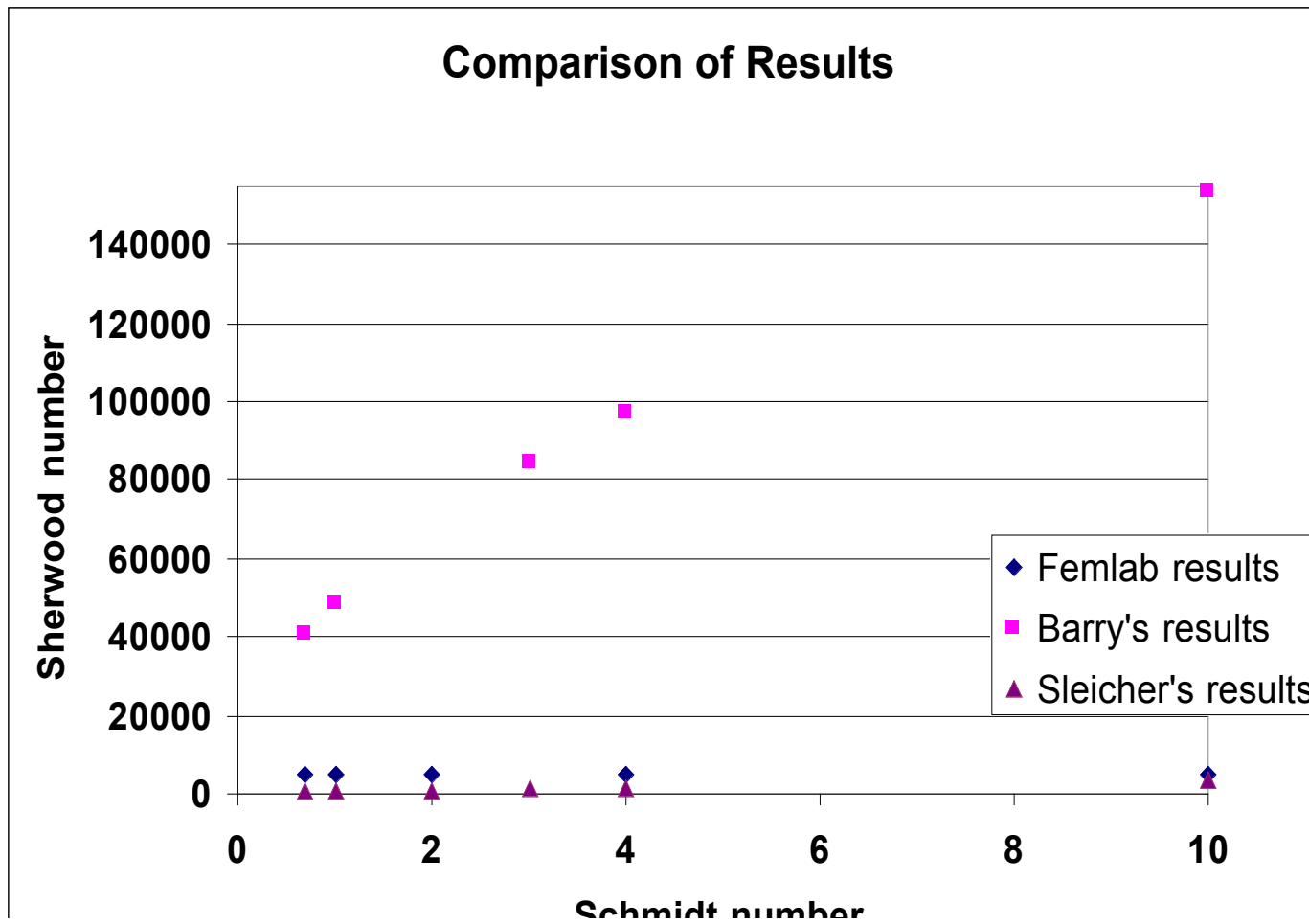
Femlab vs. Sleicher

Comparing Sh_L vs. Sc



Comparing Femlab vs. Barry

Comparing Sh_L vs. Sc



Calculating Sh_x in Femlab

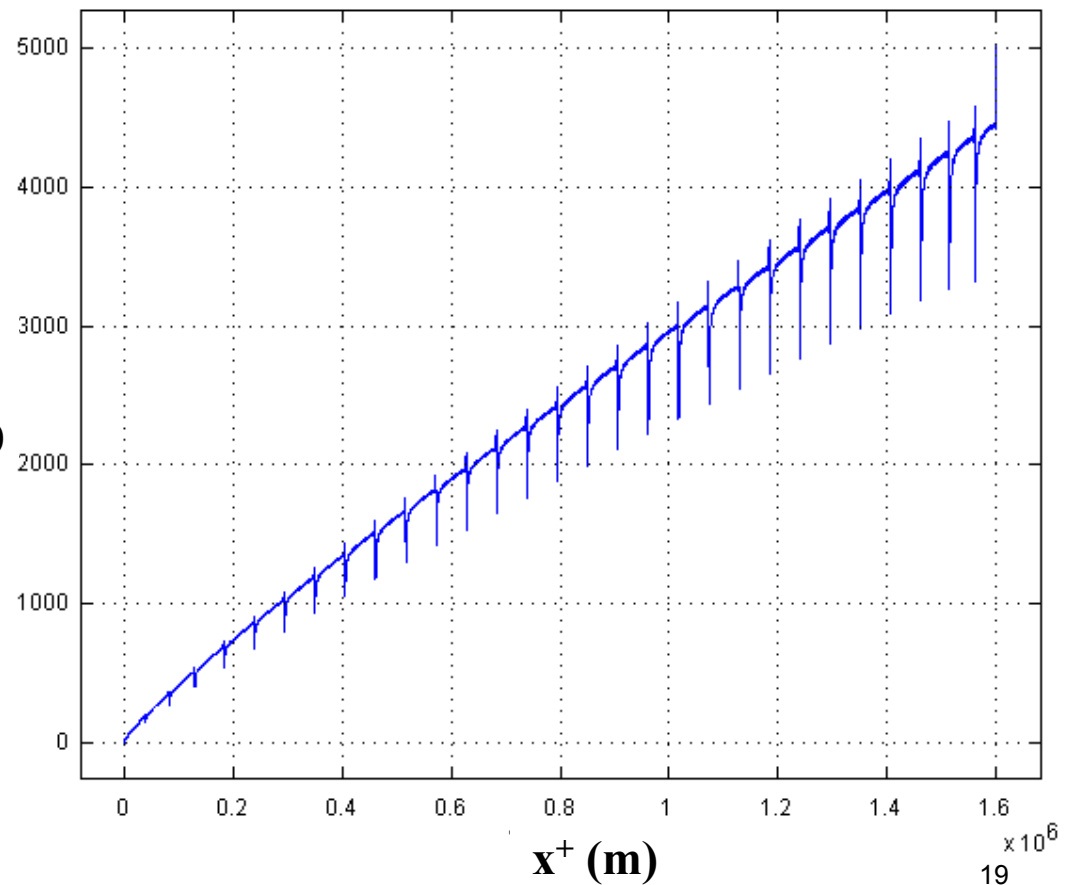
- Relate concentration to Sh_x

$$Sh_x = -x^+ \left. \frac{\partial c}{\partial y} \right|_{z^+ = 0}$$

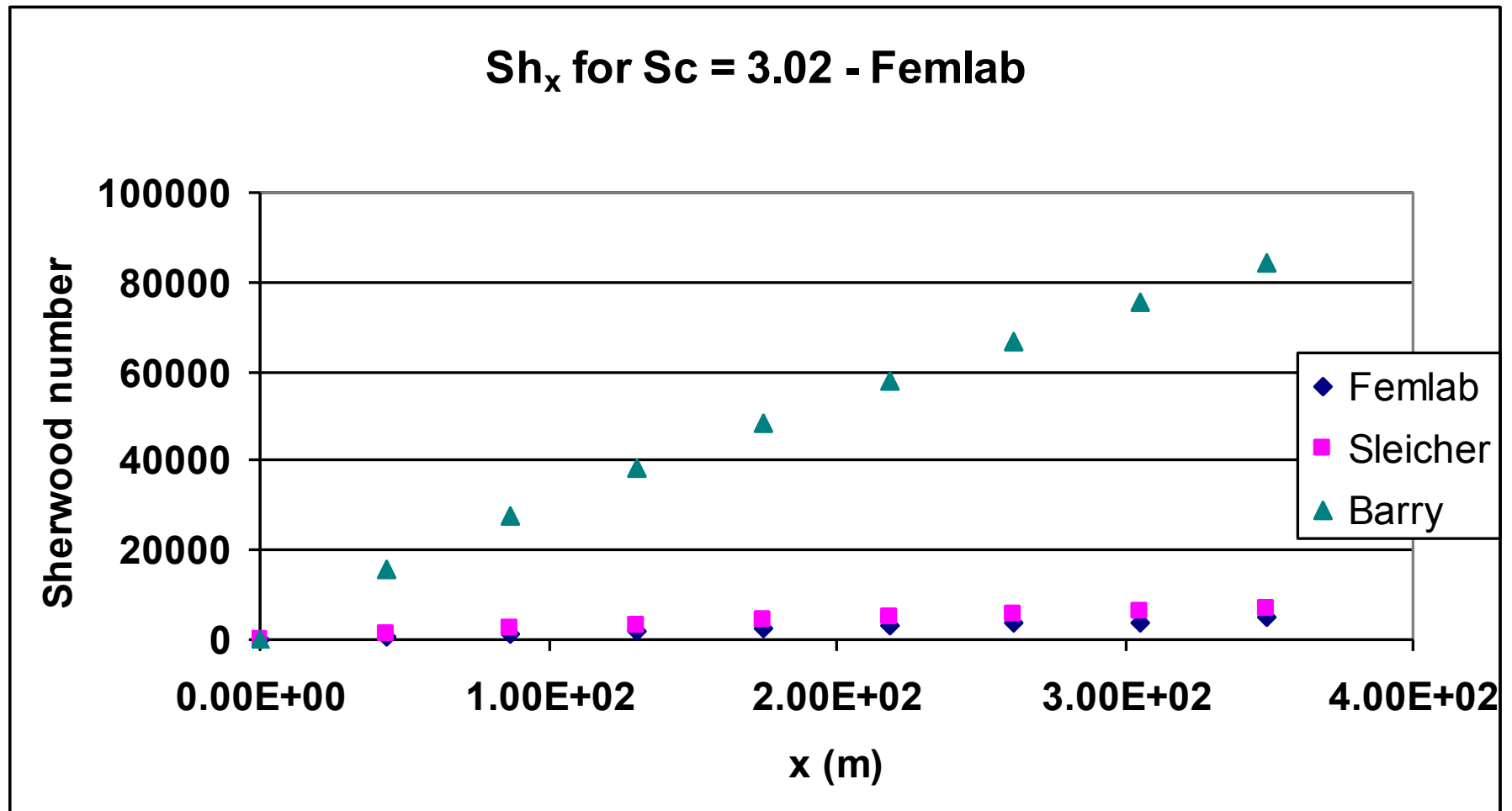
- Relate x^+ to x

$$x^+ = \frac{u_* x}{\nu}$$

Mass Flux



Comparing Sh_x





Discussion

- Comparing Femlab to Sleicher
 - Correlations are the same
 - Not as large of dependence on Sc
 - Sh_L increases faster in Sleicher's equations
- Comparing Femlab to Barry
 - Sherwood numbers VERY different
 - Sh_L increases much faster in Barry's equations

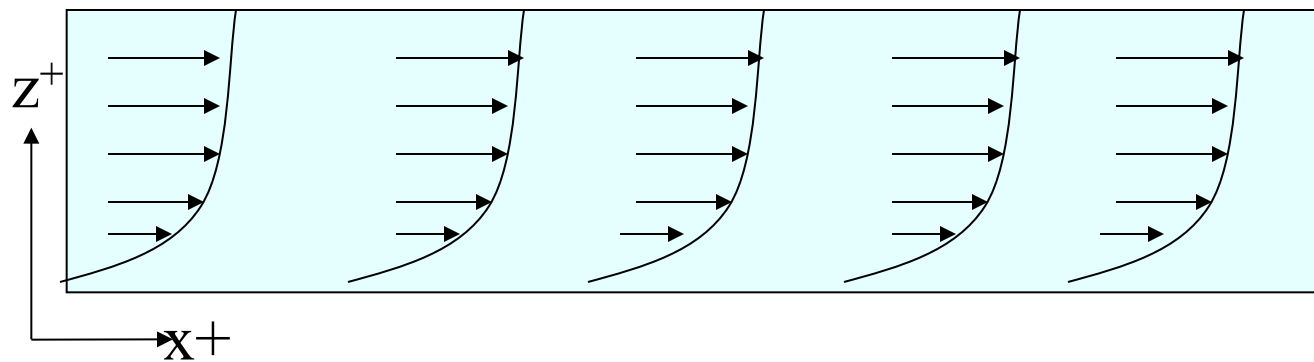


Why the deviations?

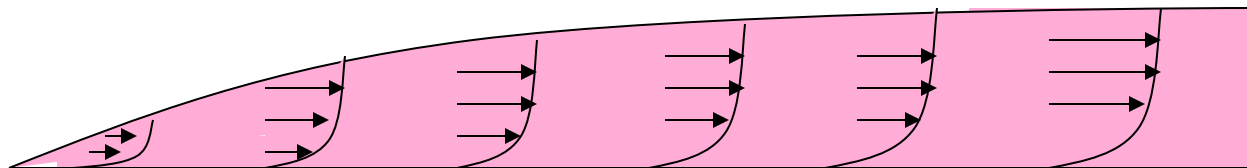
- Sleicher's numbers are different – factor $\sim 1-10$
 - Equations are based on empirical data
- Barry's numbers are different – factor $\sim 10-30$
 - Equations are based on empirical data
 - Equations apply to turbulent boundary layer
- Femlab solves differential equations analytically

Turbulent Boundary Layer explanation

Femlab = Constant velocity profile



Height $z = 8.72$ m



Height $\delta = 3.8$ m



Conclusions

- Femlab accurately models mass flux for turbulent flow
 - Depends on elements and mesh size
- Sleicher's equation shows same correlations as Femlab
 - Empirically formed equations
- Barry's equation models flow in the turbulent boundary layer regime
 - Empirically formed equations