Session 13

SIMPLE LIPID SYSTEMS

Micropipette Aspiration

- Measure non-adherent cells
 - Exhibit liquid-like flow behavior
 - Rate of entry depends on pressure
 - Exhibit surface tension behavior
 - Recovers shape upon release
- Is a fluid droplet model appropriate?
 - What is cellular viscosity?
 - What is mechanical coupling to cortex?



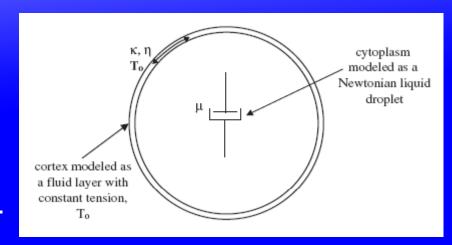
Newtonian Liquid Drop Model

Model:

 Cortical layer enclosing a Newtonian liquid

Core:

- Cytoplasm viscosity: μ
- Newtonian fluid: Stress (τ) vs. velocity gradient is linear: $\tau = \mu \; (du/dy)$



Cortex:

- Anisotropic viscous fluid layer
- Negligible bending stiffness
- Two viscosity terms
 - κ is dilation viscosity
 - η is shear viscosity

Pipet:

- Frictionless interaction
- Reaction force at pipet orifice

Approach

- Define constitutive relationship for liquid core
 - Equations of motion for Newtonian fluid with creeping flow
- Determine boundary conditions
 - Equations of motion for cortical shell (cortex)
 - Equations of viscous deformation for cortical shell
 - No slip condition at core-cortex interface

Approach

- Not an easy task to obtain numerical solution to this problem
 - Discontinuities
 - Inversion difficulties
- Yeung & Evans' approach
 - Spherical solutions exist for cell exterior to pipet
 - Course approximation used for flow inside pipet
 - Coupling provided by pressure difference:

$$\Delta P = (p_o - p_{orif}) + (p_{orif} - p_i)$$

Core: Creeping Flow

Equations of motion

$$\sigma_{ij} = -p \cdot \delta_{ij} + \mu \left[\frac{\partial v_i}{\partial x_j} + \frac{\partial v_j}{\partial x_i} \right], \tag{1}$$

By means of indicial notation, this is

$$\sigma_{11} = -p + \mu \left(\frac{\partial u_1}{\partial x_1} + \frac{\partial u_1}{\partial x_1} \right) = -p + 2\mu \frac{\partial u_1}{\partial x_1} \qquad \sigma_{22} = -p + 2\mu \frac{\partial u_2}{\partial x_2}$$

$$\sigma_{12} = \mu \left(\frac{\partial u_1}{\partial x_2} + \frac{\partial u_2}{\partial x_1} \right) = \sigma_{21} \qquad \sigma_{23} = \mu \left(\frac{\partial u_2}{\partial x_3} + \frac{\partial u_3}{\partial x_2} \right) = \sigma_{32}$$

$$\sigma_{13} = \mu \left(\frac{\partial u_1}{\partial x_3} + \frac{\partial u_3}{\partial x_1} \right) = \sigma_{31} \qquad \sigma_{33} = -p + 2\mu \frac{\partial u_3}{\partial x_3}$$

In rectilinear coordinates

$$\sigma_{11} = -p + 2\mu \frac{\partial u_1}{\partial x_1} \qquad \sigma_x = -p + 2\mu \frac{\partial u}{\partial x}$$

$$\sigma_{12} = \mu \left(\frac{\partial u_1}{\partial x_2} + \frac{\partial u_2}{\partial x_1} \right) = \sigma_{21} \qquad \tau_{xy} = \mu \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) = \tau_{yx}$$

$$\sigma_{13} = \mu \left(\frac{\partial u_1}{\partial x_3} + \frac{\partial u_3}{\partial x_1} \right) = \sigma_{31} \qquad \tau_{xz} = \mu \left(\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right) = \tau_{zx}$$

$$\sigma_{22} = -p + 2\mu \frac{\partial u_2}{\partial x_2} \qquad \sigma_y = -p + 2\mu \frac{\partial v}{\partial y}$$

$$\sigma_{23} = \mu \left(\frac{\partial u_2}{\partial x_3} + \frac{\partial u_3}{\partial x_2} \right) = \sigma_{32} \qquad \tau_{yz} = \mu \left(\frac{\partial v}{\partial z} + \frac{\partial w}{\partial z} \right) = \tau_{zy}$$

$$\sigma_{33} = -p + 2\mu \frac{\partial u_3}{\partial x_3} \qquad \sigma_z = -p + 2\mu \frac{\partial w}{\partial z}$$

Incompressibility condition for a fluid

$$\sum_{k} \frac{\partial v_k}{\partial x_k} = 0. {2}$$

By means of indicial notation

$$\frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2} + \frac{\partial u_3}{\partial x_3} = 0$$

$$\left(\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0\right)$$

 Consider one-dimensional flow (x,u). If gradient exists, then fluid density would have to expand or compress to satisfy.

Mechanical equilibrium

$$\sum_k \frac{\partial \sigma_{ik}}{\partial x_k} = 0$$

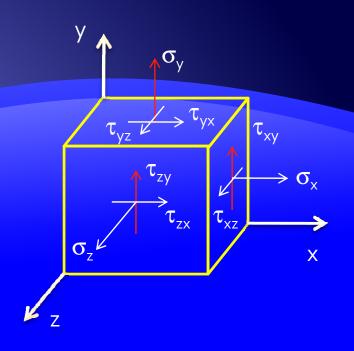
By means of indicial notation

$$\frac{\partial \sigma_{11}}{\partial x_1} + \frac{\partial \sigma_{12}}{\partial x_2} + \frac{\partial \sigma_{13}}{\partial x_3} = 0$$

$$\frac{\partial \sigma_{21}}{\partial x_1} + \frac{\partial \sigma_{22}}{\partial x_2} + \frac{\partial \sigma_{23}}{\partial x_3} = 0$$

$$\frac{\partial \sigma_{31}}{\partial x_1} + \frac{\partial \sigma_{32}}{\partial x_2} + \frac{\partial \sigma_{33}}{\partial x_3} = 0$$

$$\frac{\partial \sigma_{31}}{\partial x_1} + \frac{\partial \sigma_{32}}{\partial x_2} + \frac{\partial \sigma_{33}}{\partial x_3} = 0$$



$$\frac{\partial \sigma_{x}}{\partial x} + \frac{\partial \tau_{xy}}{\partial y} + \frac{\partial \tau_{xz}}{\partial z} = 0$$

$$\frac{\partial \tau_{yx}}{\partial x} + \frac{\partial \sigma_{y}}{\partial y} + \frac{\partial \tau_{yz}}{\partial z} = 0$$

$$\frac{\partial \tau_{zx}}{\partial x} + \frac{\partial \tau_{zy}}{\partial y} + \frac{\partial \sigma_{z}}{\partial z} = 0$$

By taking derivative of each equation (1), e.g.

$$\frac{\partial \sigma_{11}}{\partial x_1} = -\frac{\partial p}{\partial x_1} + 2\mu \frac{\partial^2 u_1}{\partial x_1^2}$$

$$\frac{\partial \sigma_{12}}{\partial x_2} = \mu \left(\frac{\partial^2 u_1}{\partial x_2^2} + \frac{\partial^2 u_2}{\partial x_1 \partial x_2} \right)$$

$$\frac{\partial \sigma_{13}}{\partial x_3} = \mu \left(\frac{\partial^2 u_1}{\partial x_3^2} + \frac{\partial^2 u_3}{\partial x_1 \partial x_3} \right)$$

Can sum together to get

$$\frac{\partial \sigma_{11}}{\partial x_1} + \frac{\partial \sigma_{12}}{\partial x_2} + \frac{\partial \sigma_{13}}{\partial x_3} = -\frac{\partial p}{\partial x_1} + \mu \left(\frac{\partial^2 u_1}{\partial x_1^2} + \frac{\partial^2 u_1}{\partial x_1^2} + \frac{\partial^2 u_1}{\partial x_2^2} + \frac{\partial^2 u_2}{\partial x_1 \partial x_2} + \frac{\partial^2 u_1}{\partial x_3^2} + \frac{\partial^2 u_1}{\partial x_1 \partial x_3} \right)$$

Simplifying by mechanical equilibrium

$$\frac{\partial \sigma_{11}}{\partial x_1} + \frac{\partial \sigma_{12}}{\partial x_2} + \frac{\partial \sigma_{13}}{\partial x_3} = -\frac{\partial p}{\partial x_1} + \mu \left(\frac{\partial^2 u_1}{\partial x_1^2} + \frac{\partial^2 u_1}{\partial x_1^2} + \frac{\partial^2 u_1}{\partial x_2^2} + \frac{\partial^2 u_2}{\partial x_1 \partial x_2} + \frac{\partial^2 u_1}{\partial x_3^2} + \frac{\partial^2 u_1}{\partial x_3^2} + \frac{\partial^2 u_1}{\partial x_1 \partial x_3} \right)$$

$$0 = -\frac{\partial p}{\partial x_1} + \mu \left(\frac{\partial^2 u_1}{\partial x_1^2} + \frac{\partial^2 u_1}{\partial x_1^2} + \frac{\partial^2 u_1}{\partial x_2^2} + \frac{\partial^2 u_2}{\partial x_1 \partial x_2} + \frac{\partial^2 u_1}{\partial x_3^2} + \frac{\partial^2 u_1}{\partial x_3^2} + \frac{\partial^2 u_2}{\partial x_1 \partial x_3} \right)$$

Simplifying by incompressibility condition

$$0 = -\frac{\partial p}{\partial x_1} + \mu \left(\frac{\partial}{\partial x_1} \left(\frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2} + \frac{\partial u_3}{\partial x_3} \right) + \frac{\partial^2 u_1}{\partial x_1^2} + \frac{\partial^2 u_1}{\partial x_2^2} + \frac{\partial^2 u_1}{\partial x_3^2} \right)$$

$$0 = -\frac{\partial p}{\partial x_1} + \mu \left(\frac{\partial^2 u_1}{\partial x_1^2} + \frac{\partial^2 u_1}{\partial x_2^2} + \frac{\partial^2 u_1}{\partial x_3^2} \right)$$

Have creeping flow eqs.

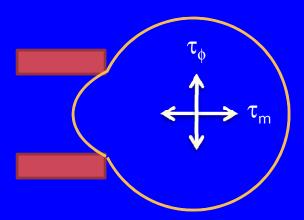
$$\frac{\partial p}{\partial x_i} = \mu \cdot \sum_k \frac{\partial^2 v_i}{\partial x_k^2},\tag{3}$$

- Stress Resultants (τ_m, τ_ϕ)
 - For thin shell, stresses integrated by thickness

$$\tau = \int \sigma_{ij} d\delta$$

- Units [N/m]
- Types: lateral, bending, torque, transverse

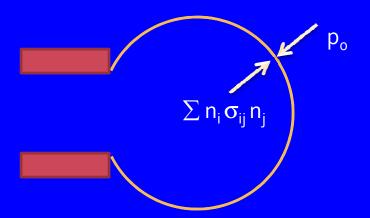
- Coordinate system: (s, θ)
 - Axisymmetry yields in-plane stress resultants
 - Meridional τ_m : $\tau_m \approx \sigma_m \delta$
 - Circumferential τ_{ϕ} : $\tau_{\phi} \approx \sigma_{\phi} \delta$



Balance of forces in normal direction

$$\Delta \sigma_n \equiv \sigma_n - \sum_{i,j} n_i \cdot \sigma_{ij} \cdot n_j = \tau_m \cdot \frac{\mathrm{d}\theta}{\mathrm{d}s} + \tau_\phi \cdot \frac{\sin\theta}{r}, \quad (4)$$

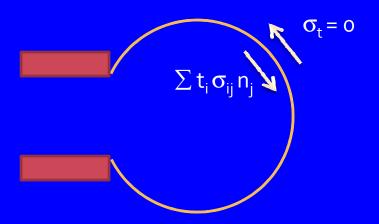
where $\sigma_n = p_o$ the outide pressure, n_i are unit vectors normal to the surface, and $\sum n_i \sigma_{ij} n_j$ are normal tractions on the interior surface by the liquid core



Balance of forces in tangential direction

$$\Delta \sigma_t = -\sigma_t + \sum_{i,j} t_i \cdot \sigma_{ij} \cdot n_j = \frac{\mathrm{d}\tau_m}{\mathrm{d}s} + \left[\frac{\tau_m - \tau_\phi}{r} \right] \cos \theta. \tag{5}$$

where σ_t = 0 on the outside, t_i are unit vectors tangential to the surface, and $\sum t_i \sigma_{ij} n_j$ are tangential tractions on the interior surface by the liquid core



- For BCs, we need constitutive relationships
- Cortex deforms by planar dilation and shear
 - κ is viscosity for surface area dilation
 - η is viscosity for shear shear
 - Units: [dyne's/cm²]*[cm] = [dyne's/cm]

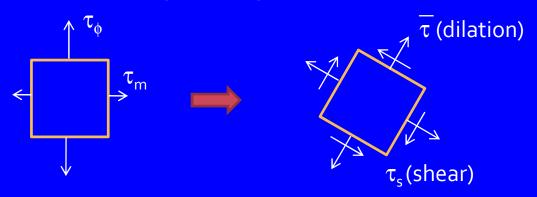
 First order model: stress resultants are proportional to rate of dilation and shear

$$\bar{\tau} \equiv (\tau_m + \tau_\phi)/2 = \bar{\tau}_o + \kappa \cdot V_\alpha$$

$$\tau_s \equiv (\tau_m - \tau_\phi)/2 = 2\eta \cdot V_s,$$
(6)

where $\overline{\tau_o}$ is static in-plane tension corresponding to zero rate of shearing and dilation

Rotation of c.s. for principal shear stresses



Kinematics of flow in the shell (curved surface)

$$V_{\alpha} = \frac{\mathrm{d}v_{s}}{\mathrm{d}s} + \frac{v_{s}}{r} \cdot \cos\theta + v_{n} \left(\frac{\mathrm{d}\theta}{\mathrm{d}s} + \frac{\sin\theta}{r} \right)$$
$$2V_{s} = \frac{\mathrm{d}v_{s}}{\mathrm{d}s} - \frac{v_{s}}{r} \cdot \cos\theta + v_{n} \left(\frac{\mathrm{d}\theta}{\mathrm{d}s} - \frac{\sin\theta}{r} \right). \tag{7}$$

where v_s, v_n are velocity fields derived from normal and tangential projections of fluid core velocities at the interface

$$\upsilon_n = \sum_k n_k \cdot \upsilon_k$$

$$\upsilon_s = \sum_k t_k \cdot \upsilon_k.$$
(8)

i.e., motion of cortical layer specified by liquid core's fluid velocities at the interface with a no-slip assumption

Solution Approach

 Yeung and Evan use a general solution for axisymmetric creeping flow for exterior region

$$v_{R}(R,\theta) = -\sum_{n=2}^{\infty} (A_{n} \cdot R^{n-2} + C_{n} \cdot R^{n}) P_{n-1}(\cos \theta)$$

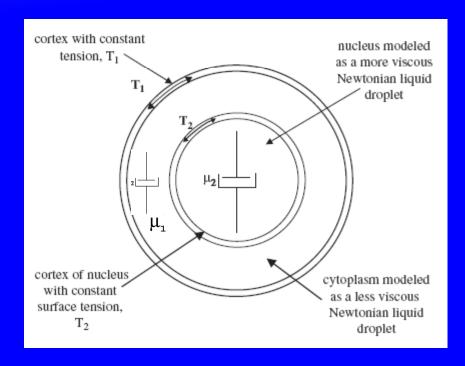
$$v_{\theta}(R,\theta) = \sum_{n=2}^{\infty} (nA_{n}R^{n-2} + (n+2)C_{n}R^{n}) \frac{I_{n}(\cos \theta)}{\sin \theta}$$

$$p(R,\theta) = \Pi - \mu \sum_{n=2}^{\infty} \frac{2(2n+1)}{(n-1)} C_{n}R^{n-1} P_{n-1}(\cos \theta), \quad (9)$$

Course approximation used for inside the pipet

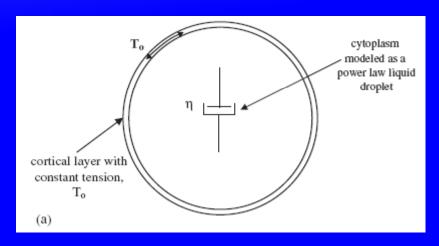
Additional models

- Compound liquid drop model
 - Incorporates the higher viscosity and stiffness of the smaller nucleus



Additional Models

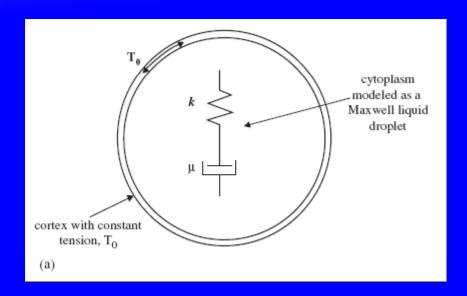
- Shear thinning liquid drop model
 - Approximates the apparent viscosity decrease with aspiration pressure



 Positive feedback: increase in shear rate leads to decreased viscosiy, which in turn further increases shear rate...

Additional Models

- Maxwell Liquid Drop
 - Large deformations satisfied by Newton liquid drop model but not for small deformations



Accounts for initial elastic-like entry during aspiration