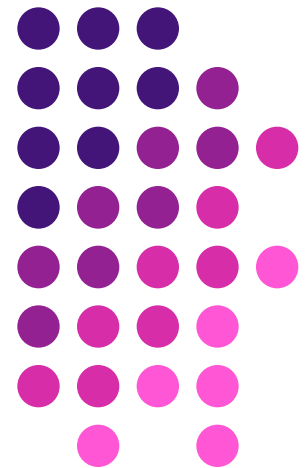


Pressure Drop of Gases in Contractions and Expansions in Microchannels

Kaarin Dawes

ChemE 499

Spring 2003





Objectives

- Determine pressure drop due to an expansion or contraction
- Determine equivalent length
- Compare results to LWZ paper



Background

- Solve Navier-Stokes equations in 3-D

- $\rho u \cdot \nabla u = -\nabla p + \mu \nabla^2 u$

- Check Perry's equation for incompressible flow

- $Q = \frac{WH^3 \Delta P}{K\mu L}$

- Compute results using LWZ equation

- $\dot{m} = \frac{H^3 W P_o^2}{24 R T L \mu} \left[\left(\frac{P_i}{P_o} \right)^2 - 1 + 12 K n_o \left(\frac{P_i}{P_o} - 1 \right) \right]$



Geometry (45°)

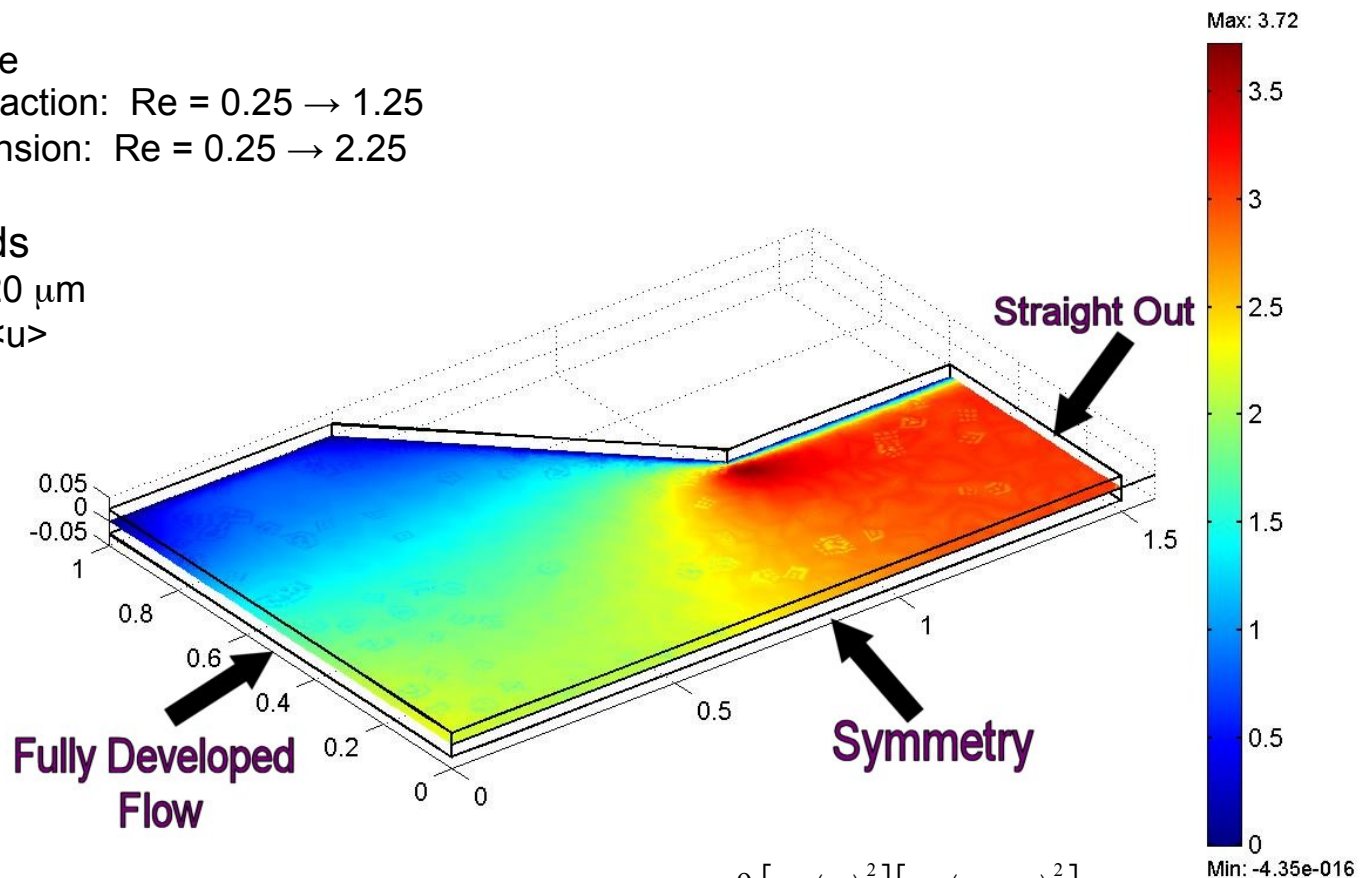
- Subdomain

- $\mu = 1$
- $\rho = \text{Re}$
- Contraction: $\text{Re} = 0.25 \rightarrow 1.25$
- Expansion: $\text{Re} = 0.25 \rightarrow 2.25$

- Standards

- $x_s = 20 \mu\text{m}$
- $u_s = \langle u \rangle$

$\text{Re}(5)=1.25$ Slice: x velocity (u)



Inlet Velocity Profile:
$$u(x) = \frac{9}{4} \left[1 - \left(\frac{y}{1} \right)^2 \right] \left[1 - \left(\frac{z}{0.025} \right)^2 \right]$$

Geometry (90°)



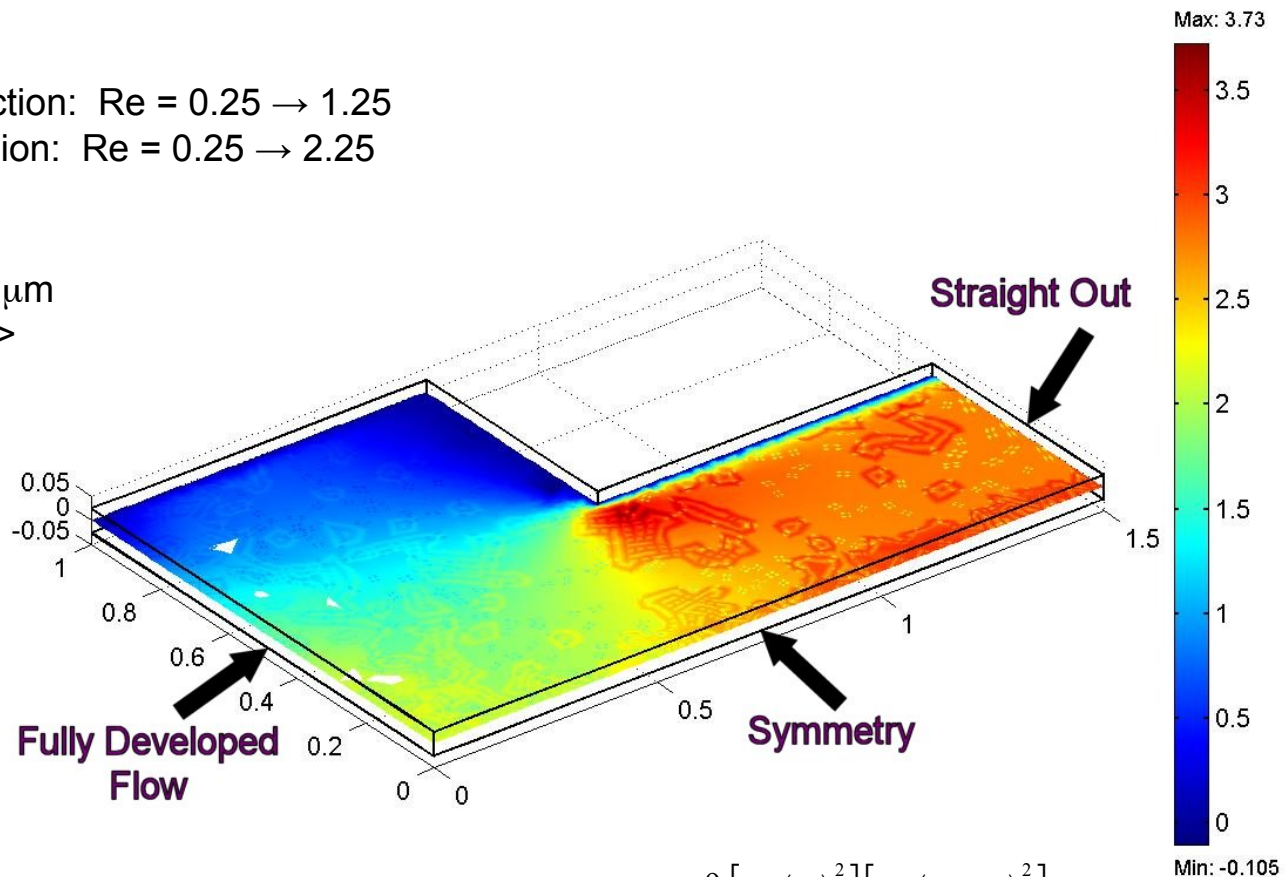
- Subdomain

- $\mu = 1$
- $\rho = \text{Re}$
- Contraction: $\text{Re} = 0.25 \rightarrow 1.25$
- Expansion: $\text{Re} = 0.25 \rightarrow 2.25$

- Standards

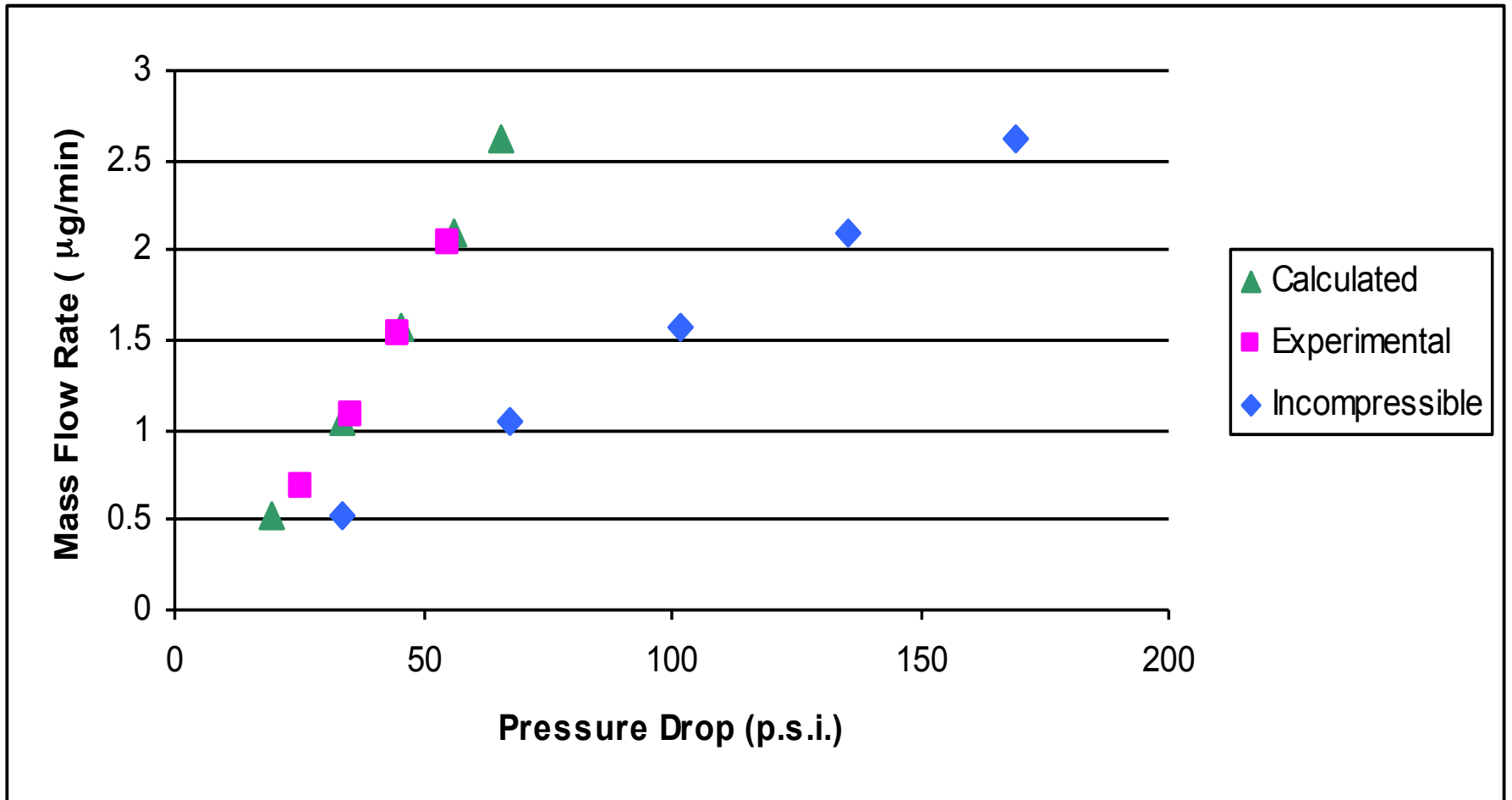
- $x_s = 20 \mu\text{m}$
- $u_s = \langle u \rangle$

Re(5)=1.25 Slice: x velocity (u)

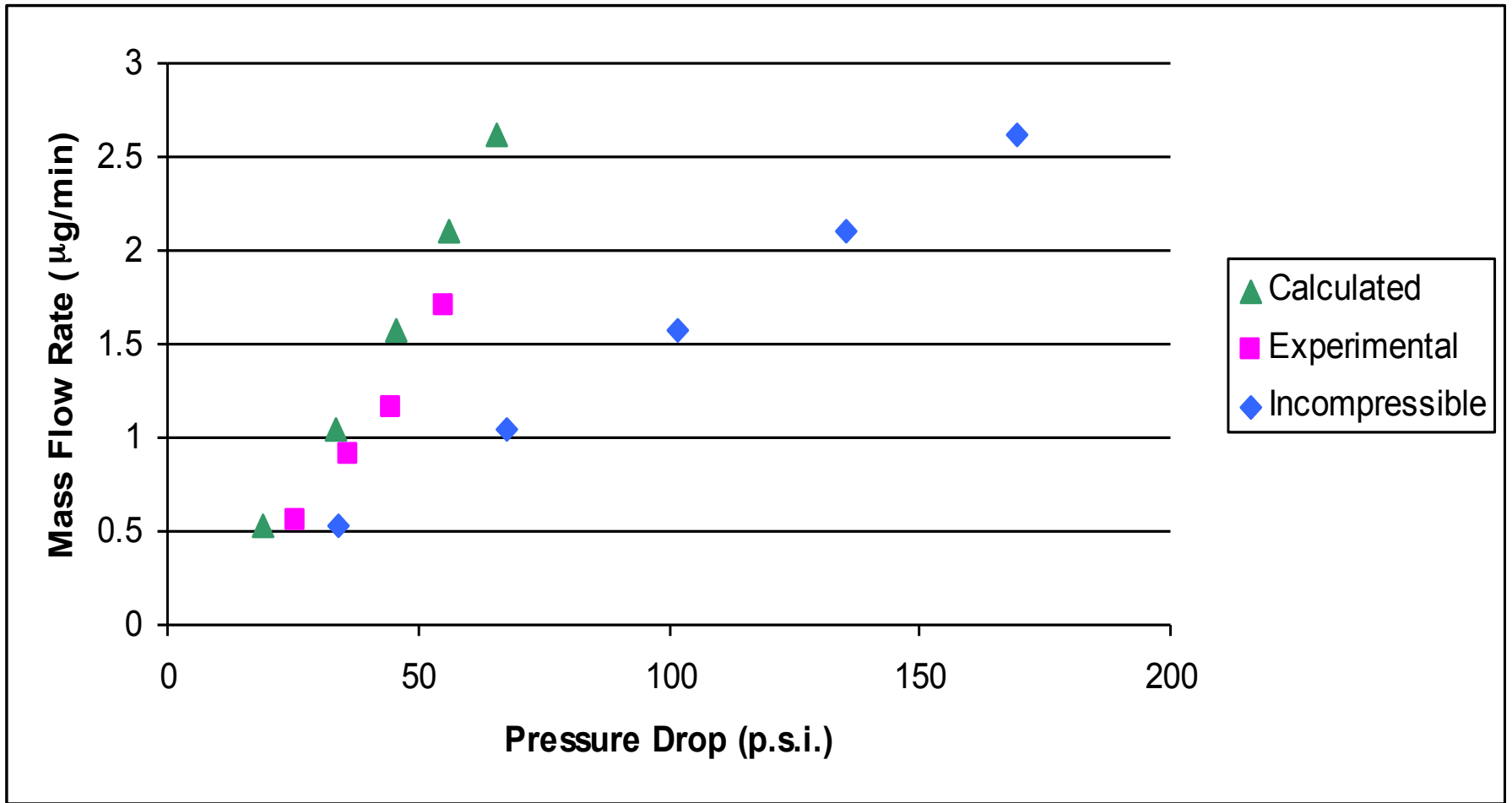


Inlet Velocity Profile:
$$u(x) = \frac{9}{4} \left[1 - \left(\frac{y}{1} \right)^2 \right] \left[1 - \left(\frac{z}{0.025} \right)^2 \right]$$

45° Contraction



90° Contraction



Contribution to Total Pressure Drop



Flow Rate ($\mu\text{g}/\text{min}$)	0.525	1.05	1.575	2.10	2.625
ΔP_{tr} (psi)	0.2857	0.5714	0.8571	1.1428	1.4286
Percentage of Total Pressure Drop	1.48%	1.70%	1.88%	2.03%	2.17%

Data from 45° contraction, slightly larger for 90° contraction

Equivalent Length



Angle	45° Contraction	45° Expansion	90° Contraction	90° Expansion
Calc' d Length (μm)	54.3	55.5	58.0	59.7
LWZ Length (μm)	500	650	1100	1200



Mesh Comparison

Mesh	Extremely Coarse	Coarser	Normal	Finer
ΔP_{tr} (psi)	0.2857	0.2838	0.2837	0.2836
% difference	--	-0.65	-0.70	-0.73
ΔP_t (psi)	19.267	19.265	19.265	19.265
% difference	--	-0.01	-0.01	-0.01
L_e (μm)	53.5	53.2	53.1	53.1
% difference	--	-0.65	-0.70	-0.73

Data from 45° contraction



Conclusions

- Flow cannot be modeled as incompressible
- Pressure drop due to expansion/contraction is very small part of total pressure drop
- LWZ equivalent lengths seem exaggerated